

# QbD Based Process Development Strategies for Antibodies

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#### ABOUT COOK PHARMICA



- CONTRACT DEVELOPMENT AND MANUFACTURING ORGANIZATION
- WHOLLY-OWNED SUBSIDIARY OF COOK MEDICAL
- LEGACY OF LIFE SCIENCES INNOVATION SINCE 1963
- 900,000 FT<sup>2</sup> (83,600 M<sup>2</sup>) FACILITY IN BLOOMINGTON, INDIANA USA

#### THE ONE SOURCE, ONE LOCATION MODEL



# CLINICAL AND COMMERCIAL

#### DEVELOPMENT

PROCESS DEVELOPMENT ANALYTICAL DEVELOPMENT FORMULATION DEVELOPMENT

#### DRUG SUBSTANCE

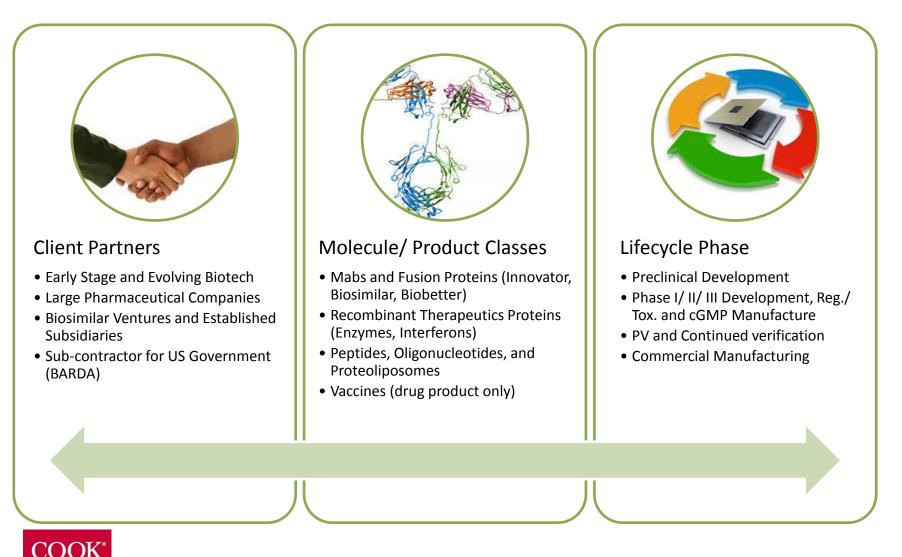
CELL CULTURE MANFACTURING CAPACITY TO 250 L, 600 L, (2) 2,500 L

#### DRUG PRODUCT

BARRIER ISOLATOR TECHNOLOGY VIAL FILLING LYOPHILIZATION SYRINGE FILLING SAFETY DEVICE AND AUTOINJECTOR ASSEMBLY BLISTER THERMOFORMING KITTING AND CARTONING



#### **GROWTH IN DIVERSITY OF PROJECTS AND CLIENTS**

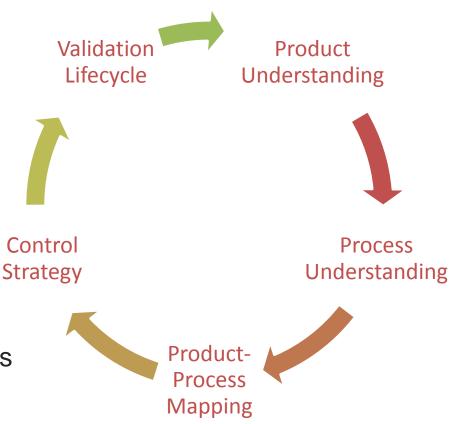




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#### PRESENTATION OUTLINE

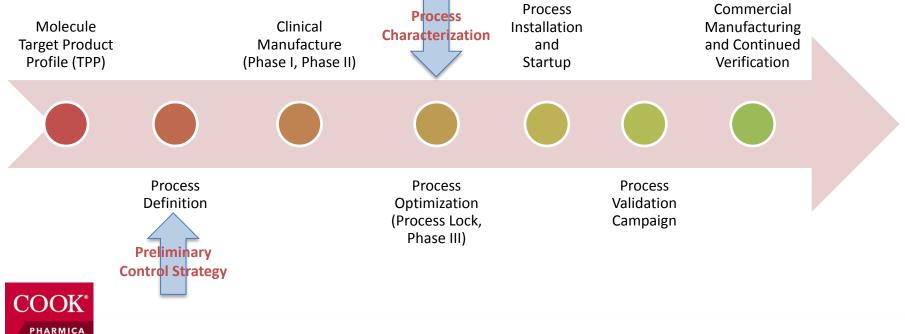
- mAb Molecule to Market Lifecycle
- Product Understanding
  - Criticality Assessments
  - Preliminary Analytical Control Strategy
- Process Understanding
  - Risk Management
  - Process Characterization
- Product-Process Mapping
  - Design Space
  - CPP-CQA Linkages
- Control Strategy PV Readiness with well-defined/ wellcharacterized process





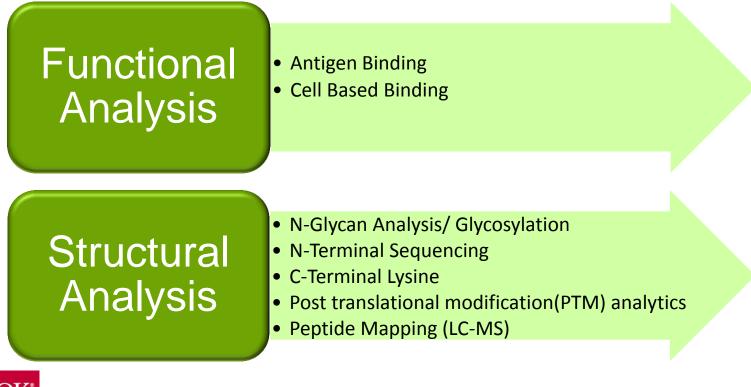
#### MOLECULE TO MARKET

- Process Definition (Phase I, Phase II)
  - In-Depth Product Characterization but little or no process characterization
  - Preliminary Control Strategy and Process Definition for meeting TPP
  - Initial scale-up for GMP Manufacture
- Process Optimization (Phase III)
  - In-depth process characterization
  - DOE Driven Studies and establish Design Space
  - Final Scale-up and process lock
  - Establish Control Strategy



#### **PRODUCT UNDERSTANDING: IN-DEPTH CHARACTERIZATION**

Prior to early development, in-depth molecule characterization supports criticality risk assessment of product quality attributes and insight into stability





#### PRELIMINARY CONTROL STRATEGY

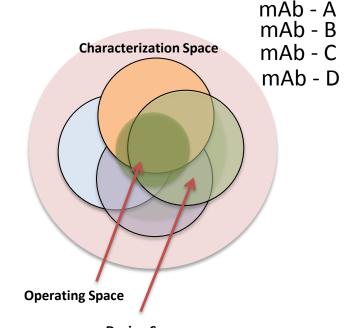
Based on a criticality risk assessment, a testing plan based on criticality of product attributes is established (One or more analytical methods associated with each CQA)

	Critical Quality Attribute	Analytical Methods	Analytical Control Strategy				
			In- Process	Release	Stability	Char.	
≻	lgG	Protein A - HPLC	х	х			
≻	Protein Concentration	UV-A280	х	x	x		
≻	Protein ID	Peptide mapping (LC-MS)		x		х	
≻	Functional Analysis	ELISA Binding ; Cell-Based Assays				х	
>	Product-related Impurities (DNA, Protein A, HCP)	ELISA based Methods	x	x			
>	Adventitious Agents (Bioburden, Endotoxin)	Plate Count Methods, LAL	x	x			
>	Charge Variants (Deamidation, Sialylation, etc.)	IEX-HPLC, cIEF/ iCE	x	x	x	x	
	Size Variants (aggregation, dimers, fragmentation)	SEC-HPLC , SDS-PAGE, CE-SDS	x	x	x	x	
≻	Process Impurities (Triton X-	RP-HPLC	x	x			
	100, residual solvents, etc.)	GC	x	х			
>	Glycan Profile	FL-HPLC, MALDI MS					



#### PROCESS DEFINITION – A TECHNOLOGY PLATFORM APPROACH

- A key strategy for success and quick turnaround is an established development platform
  - Standardized processes with established design space
  - Well-characterized standard equipment, resins etc. with established scale-up criteria and engineering design space
- An established technology platform allows for significantly reduced parameter screening to develop a process for a class of molecules that meets product TPP and provides assurance of quality
  - No loss of flexibility with appropriate technology platform



Design Space

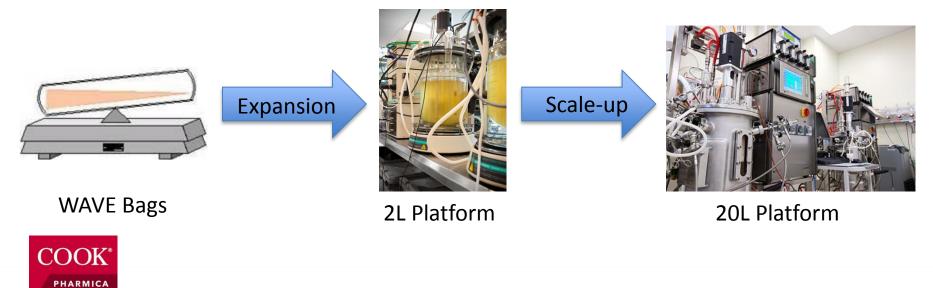
Concept in harmony with QbD – A Systematic Approach to Leveraging Prior Knowledge...



#### **PROCESS DEFINITION – UPSTREAM DEVELOPMENT**

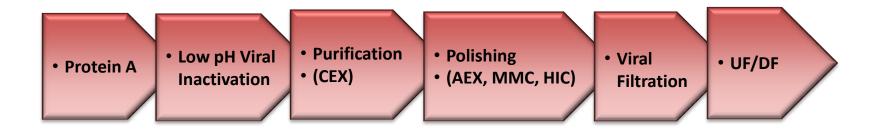
# Cell Culture Platform

- Standard cell expansion processes (e.g. WAVE<sup>®</sup> bags)
- Standard Off-the-shelf media options with baseline feed strategy
- 2L and 20L platform with established design charts for scale-up
- Standardized processes: Feed Strategy, Inoculation Density, Temperature shift, pH/ pCO2 control, Gassing Strategy etc.
- Minimal experimentation to establish high titer process and meet critical product attributes and target product profile



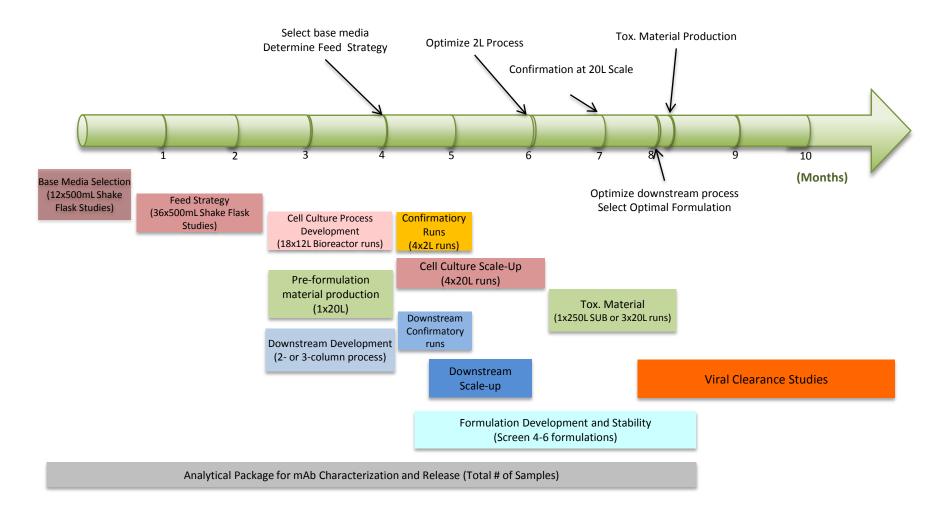
# **Downstream Platform**

- Standard 2 or 3 column process
- Well-characterized resin library and established vendors
- Established column packing and operation and scale-up criteria
- Established viral filtration technologies
- Minimal screening experiments to establish baseline process to meet in-process controls and product attributes





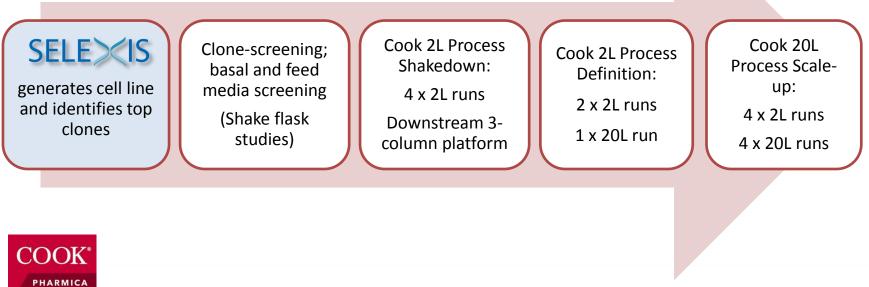
## TYPICAL DEVELOPMENT PROGRAM FOR EARLY PHASE MOLECULES



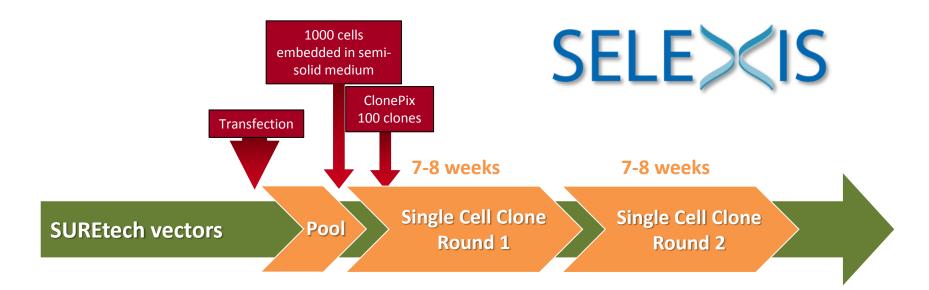


### CASE STUDY – RAPID DEVELOPMENT OF A BIOSIMILAR

- Background
  - Collaboration with SELEXIS for a biosimilar trastuzumab (model molecule), using a client-owned SELEXIS cell line for demonstrating proof-of-concept.
- Objective
  - Create scalable process via a technology platform approach for commercial-ready titers with minimal development
- Approach



#### MAMMALIAN CELL LINE DEVELOPMENT PLATFORM



#### Generation of high performance and stable cell lines using the SURE*technology* Platform<sup>™</sup> for cGMP manufacturing

- SGE high-productivity expression vector
- Single-cell cloning in chemically-defined media
- Suspension growth in chemically-defined basal media (commercial media)
- Optimized feed strategy (commercial feed)
- Robust growth to high cell densities

#### **Candidate Clones**

- Productivity assay
- Functional assay
- Manufacturing
- Preclinic/tox

#### **Clonal Cell Lines**

- Fed batch process
- cGMP manufacturing
- Clinical trial supply
- Market supply
- Research cell bank

#### INITIAL SHAKE FLASK STUDIES: FEED STRATEGY SCREENING WITH FULL FACTORIAL DOE

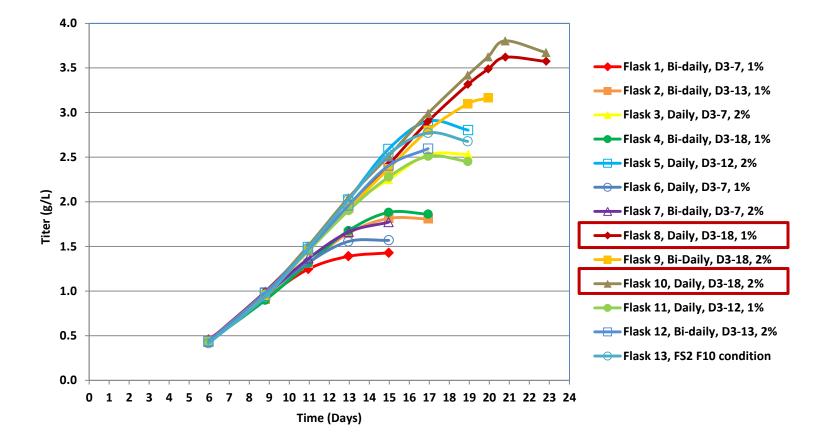
Variables							
Feed Concentration		1% 2		2%		NA	
Feed Frequency			Daily	Bi-daily		NA	
Feed Timing			D3-7	D3-12/13		D3-18	
	Concentratio	n	Frequen	су	Timing	g	
		1	Bi-daily		D3-7		
		1	Bi-daily		D3-12	/13	
		2	Daily		D3-7		
		1	Bi-daily		D3-18		
		2	Daily		D3-12	/13	
		1	Daily	D3-7			
		2 Bi-daily D3-7					
		1 Daily D3-18					
		2	Bi-daily		D3-18		
		2	Daily		D3-18		
		1	Daily		D3-12	/13	
		2	Bi-daily		D3-12	/13	

 $\rightarrow$  12 flask DoE full factorial 0.7 0.6peak 0.0 (g) 0.3-0.2-25 15 10 20 30 35 5 n Total Feed Amount (%) 16%

Non-linear relation between total feed amount and production → 16-20% best range for good titer with reduction in wasted feed (cost) JMP analysis indicates daily feeds D3-18 best



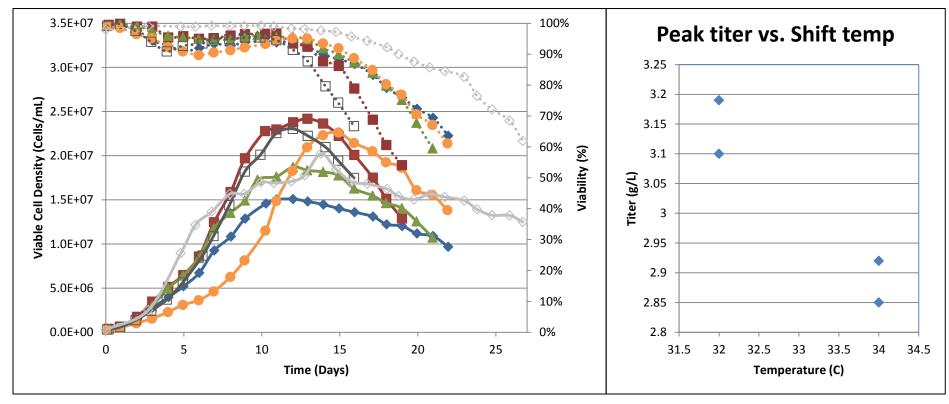
#### **RESULTS – TITER DRIVEN OPTIMIZATION OF FEED STRATEGY**

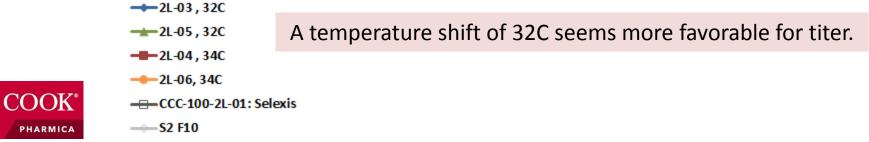


Daily Feed of 1% and 2% are top performers for titer



#### 2L PROCESS SHAKEDOWN – UNIVARIATE STUDY WITH TEMPERATURE SHIFT





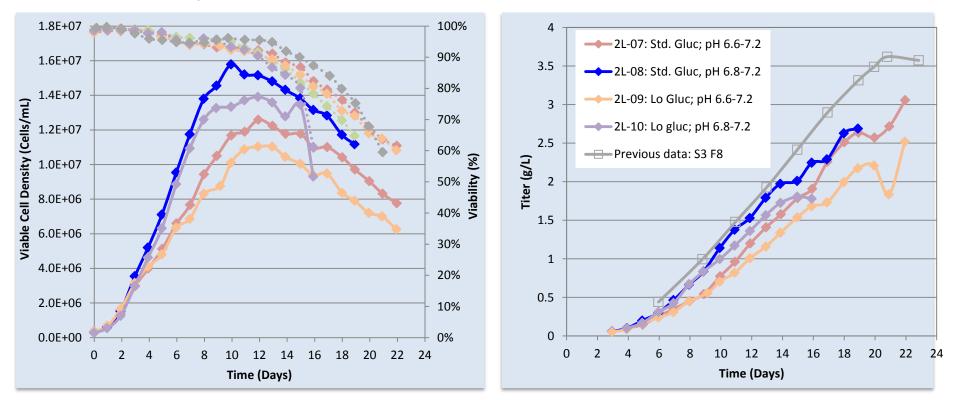
### 2L PROCESS DEVELOPMENT: DEFINE PH AND GLUCOSE LEVELS

#### **Factors Tested:**

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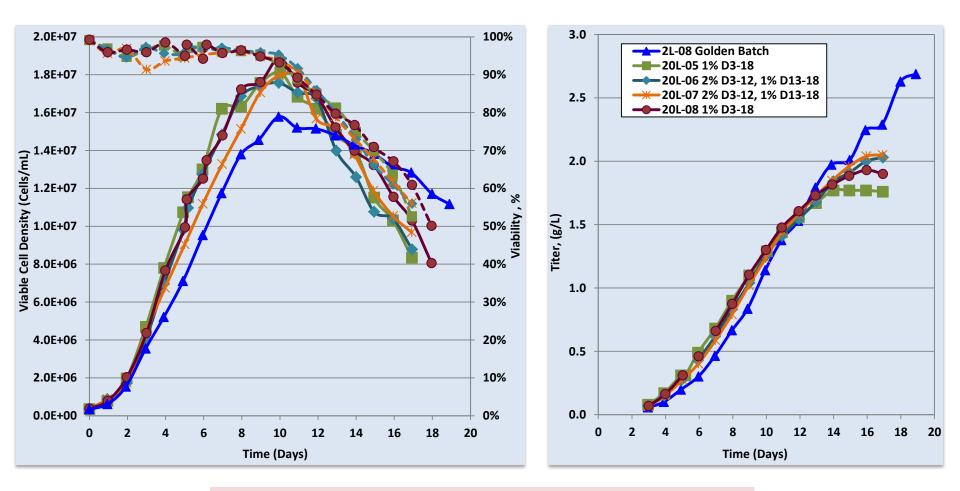
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- Low Glucose vs Std. Glucose Levels
- pH range 6.6 7.2 vs 6.8 7.2



**Results**: Maintaining pH above 6.8 early benefits cell growth, but shortens culture longevity; Standard glucose levels gives better titer

### PROCESS CONFIRMATION AND SCALE-UP

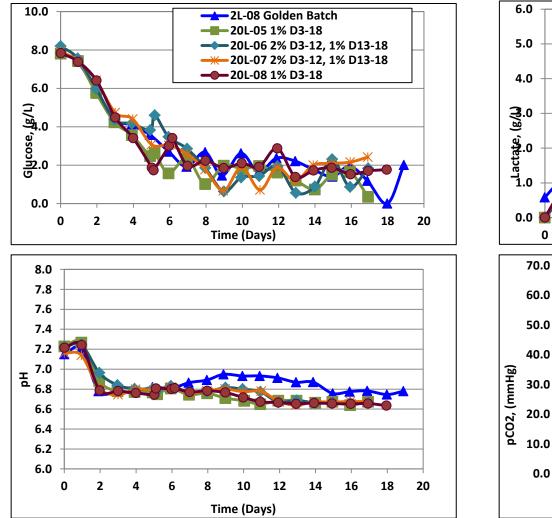


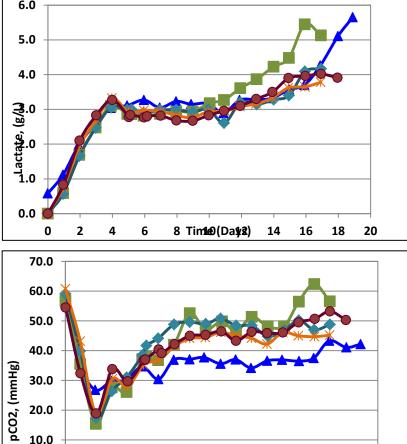
2L-08 baseline condition – "Golden Batch"



• Scale up to 20L

#### PROCESS SCALE-UP: METABOLITE PROFILES

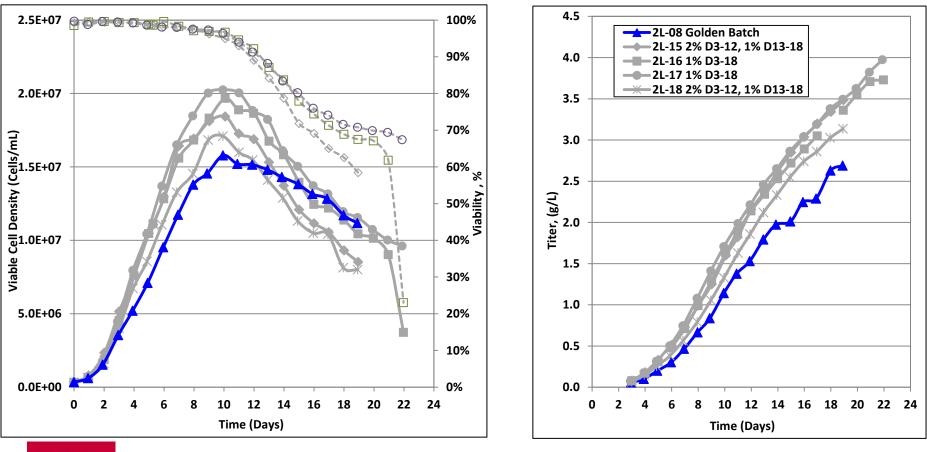




Time (Days)

#### HIGH TITER PROCESS DEVELOPMENT – WORK IN PROGRESS

- Optimized seed train in 2L
- Diluted vs concentrated feeds
- Additional work required for optimization of 20L process



#### DOWNSTREAM PROCESS – DEVELOPMENT AND SCALE-UP RESULTS

# Standard 3-column process

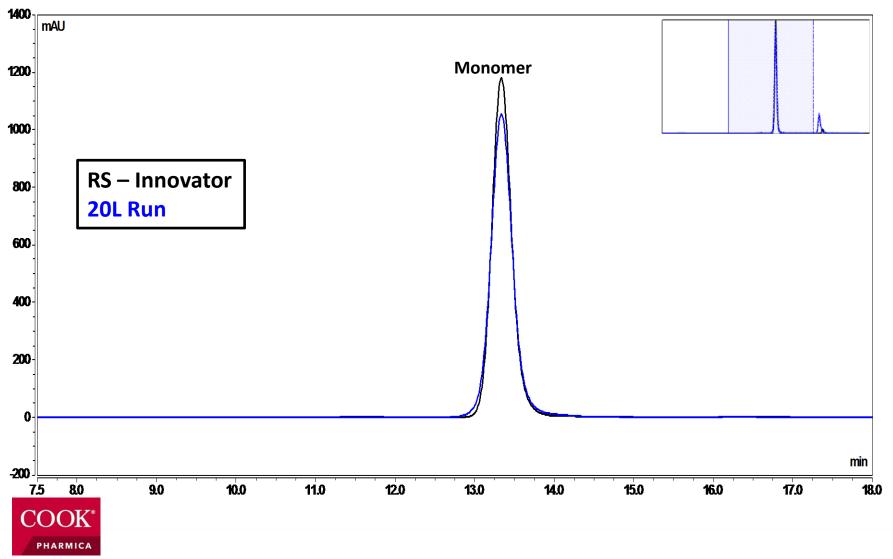


#### Results from a pilot scale downstream process for a 20L scale bioreactor run:

Process Step	Pool Conc. (g/L)	Pool Vol. (L)	Total g	Step Yield (%)	SEC-HPLC Monomer (%)	HCP by ELISA (ng/mg)
Clarified Harvest	1.59	18.91	30.61	100	NA	NA
MabSelect Sure/Viral Inactivation Cycle 1	4.29	3.4	14.57	93.8	96.4	1075.4
MabSelect Sure/Viral Inactivation Cycle 2	4.22	3.25	13.72	94.4	96.6	NA
Combined Viral Inactivation Pool*	4.26	5.67	24.15	NA	95.1	962.8
POROS XS Pool**	6.09	3.4	20.73	87.5	99.1	3.9
POROS Q Pool	1.02	17.76	18.12	99.7	99.9	< 1
Viral Filtration Pool	0.96	19	18.24	100.7	99.8	< 1
UFDF Pool	21.89	0.82	18.06	99.0	99.1	< 0.05



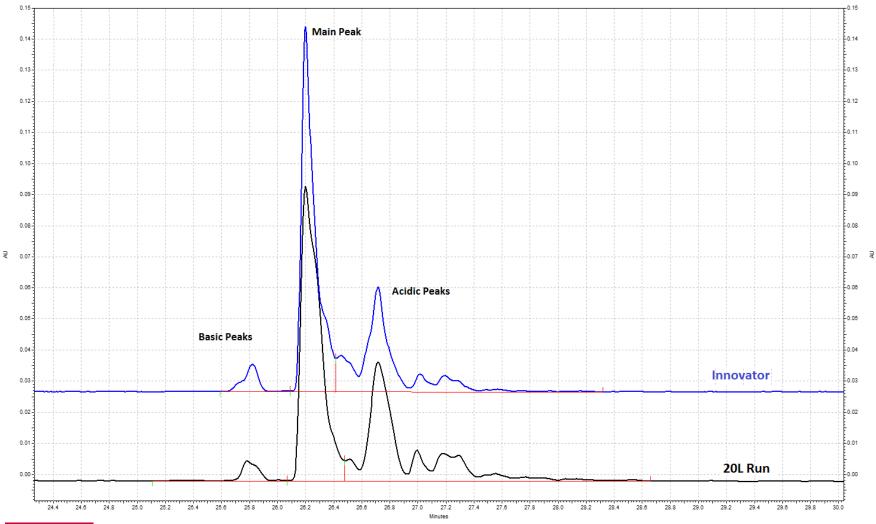
#### **RESULTS:** SIZE VARIANTS BY SEC-HPLC



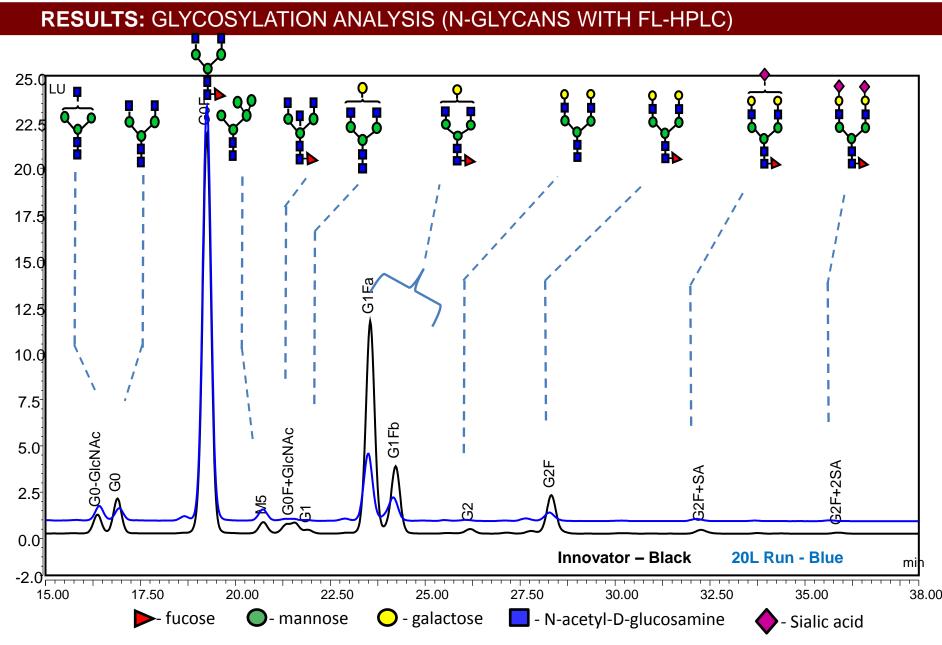
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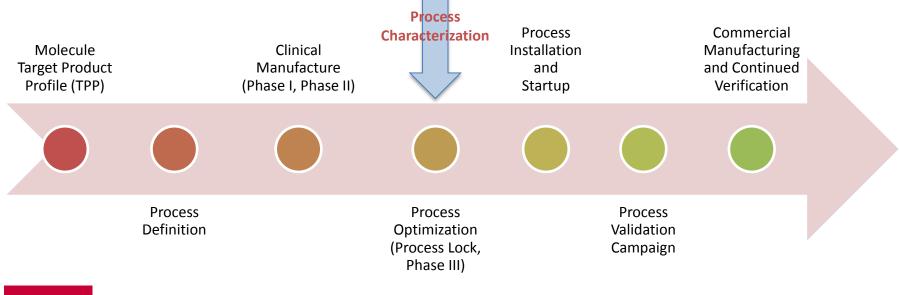
## **RESULTS:** CHARGE VARIANTS BY CIEF



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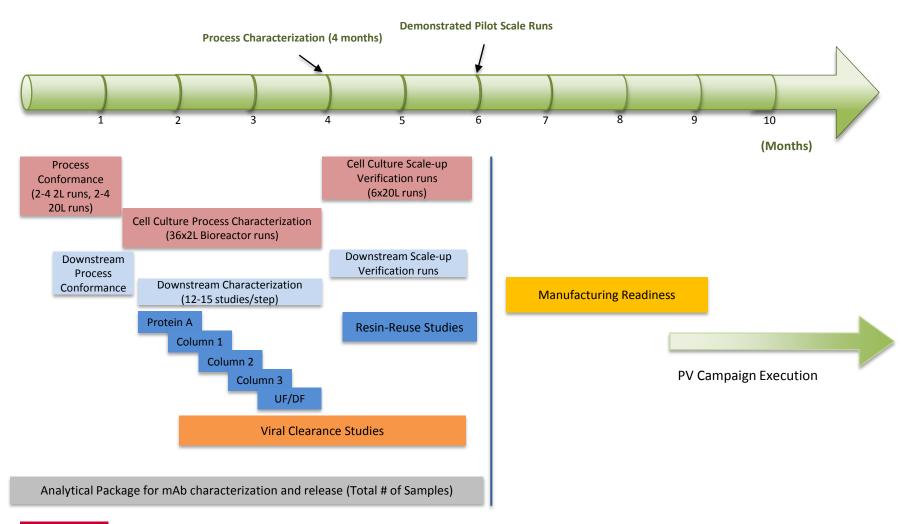
#### MOLECULE TO MARKET

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## MONOCLONAL ANTIBODY CHARACTERIZATION APPROACH





#### EXAMPLE PROCESS CHARACTERIZATION DOE FOR A CEX STEP FOR TRASTUZUMAB

- Cation Exchange Chromatography
  - POROS XS<sup>®</sup> Resin in Bio-Rad smallscale column (1.2 – 1.3 mL CV)
- Method
  - Equilibration: 10 mL of 50 mM Sodium Acetate
  - Load: pH and conductivity adjusted material
  - Equilibration Wash: 10 mL of 50 mM Sodium Acetate
  - Salt Strip: 10 mL of 50 mM Sodium Acetate, 500 mM NaCl

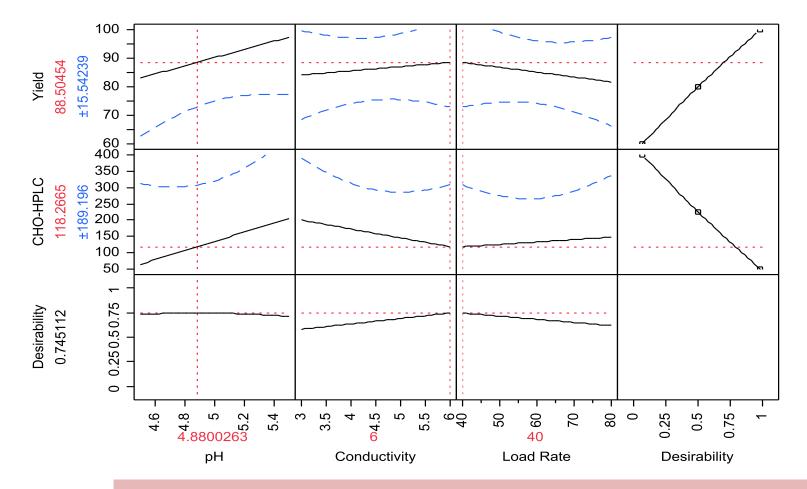
Column #	Pattern	рН	Conductivity	Load Rate
1		4.5	3	40
2	000	5	4.5	60
3	+++	5.5	6	80
4	+-+	5.5	3	80
5	+	5.5	3	40
6	-++	4.5	6	80
7	+	4.5	3	80
8	-+-	4.5	6	40
9	++-	5.5	6	40

#### Full Factorial Screening Design:

- Factors: pH, Conductivity, Load Rate
- Response: Yield, CHO-HCP Level



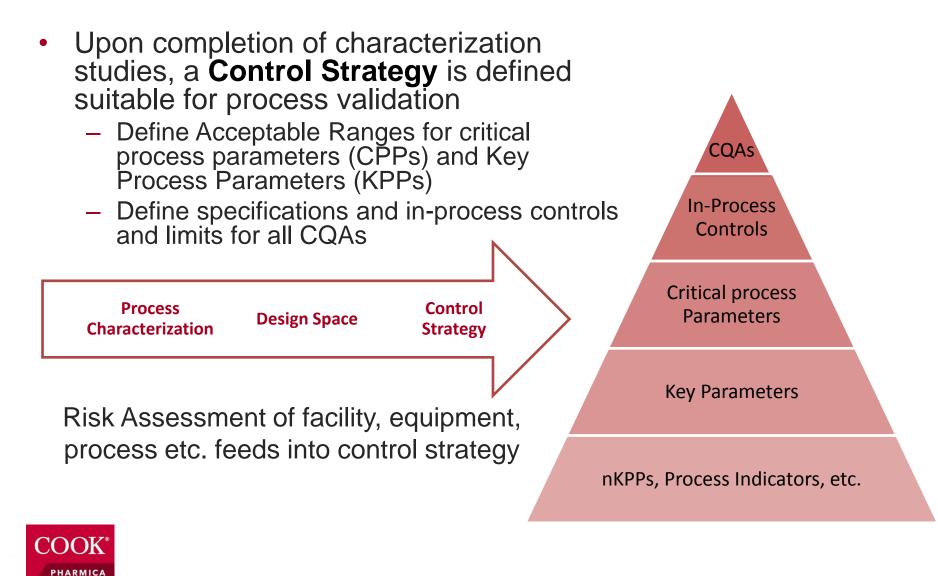
#### STATISTICAL ANALYSIS: PREDICTION PROFILER – MAXIMIZING DESIRABILITY



<u>Target Operating Range</u>: pH operating Space based on maximum desirability. Acceptable range defined depending on desired HCP clearance (Additional Optimization DOE studies required)



#### DEFINE CONTROL STRATEGY - MANUFACTURING READINESS FOR PV





- A flexible technology platform allows for rapid development for early phase clinical manufacturing
  - Leverage prior knowledge and experience
  - Reduced parameter screening
  - Well-characterized equipment, resin library and methods
- Phase-appropriate QbD as a critical enabler for successful validation and robust process – molecule to market
  - Process characterization as part of late stage development



#### ACKNOWLEDGMENTS

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